



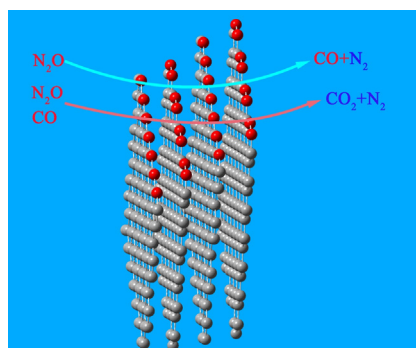
Research Paper

Theoretical research on heterogeneous reduction of N₂O by charZhengyang Gao^a, Weijie Yang^{a,*}, Xunlei Ding^b, Yi Ding^a, Weiping Yan^a^aSchool of Energy and Power Engineering, North China Electric Power University, Baoding 071003, China^bSchool of Mathematics and Physics, North China Electric Power University, Beijing 102206, China

HIGHLIGHTS

- The heterogeneous reduction mechanism of N₂O by char is revealed.
- Char provides free sites and reduces the energy barrier of N₂O reduction.
- The char edge structure has a notable influence on N₂O decomposition.
- The participation of CO can reduce activation energy of N₂O reduction.

GRAPHICAL ABSTRACT



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ABSTRACT

In order to investigate heterogeneous reduction of N₂O by char, quantum chemistry theoretical calculation based on zigzag and armchair char edge model was conducted. Thermodynamics and kinetics calculation were carried out combined with density functional theory (DFT) and conventional transition state theory (TST). Theoretical calculation results indicate that heterogeneous reduction of N₂O by char undergoes two stages: N₂O decomposition on char edge and residual oxygen desorption from char edge. N₂O decomposition process is an exothermic reaction and takes place spontaneously and irreversibly. Char acts as an important catalyst which not only provides free sites for the heterogeneous reduction but also reduces the reaction energy barrier. The participation of CO can significantly reduce reaction activation energy of residual oxygen desorption. The char edge structure has notable influence on activation energy of N₂O decomposition on char edge. Activation energy values of N₂O decomposition on zigzag and armchair char edge are 33.91 kJ/mol and 163.58 kJ/mol, respectively. The calculation results can not only deepen understanding of the reaction mechanism but also provide theoretical guidance for operation optimization of low N₂O emission.

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1. Introduction

Nitrogen oxides (NO_x) emits from coal combustion is a major environmental pollutant, which can result in the greenhouse effect, the depletion of the ozone layer, the formation of acid rain and the generation of photochemical smog. Nitric oxide (N₂O) is a major

pollutant of NO_x, particularly in circulating fluidized bed boiler (CFBB) [1]. N₂O emission from coal-fired CFBB is at range of 50–200ppm [2], with an 0.2–0.4% growth rate every year.[3] Potential damage of N₂O to environment leads to an intense research on efficient removal of N₂O.

Extensive experimental studies on N₂O suggest that char and some metal oxides have strong N₂O reduction ability [4–13] and the reduction mainly derives from heterogeneous reactions [14]. Limestone (CaCO₃) addition to coal-fired boiler could contribute

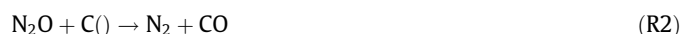
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to a decrease of N₂O emission, because limestone can promote the decomposition of N₂O [4]. Some metal oxides [5–8] (SiO₂, Al₂O₃, CaO, MgO and Fe₂O₃) in char and metal based zeolite [9,10] can also catalyze N₂O reduction, and N₂O reduction by metal oxides can be described as followings [11]:



Compared with metal oxides, char has more prominent effect on N₂O decomposition. Wang et al. [12] compared the effects of major metal oxides and fixed carbon in char on N₂O reduction and suggested that contribution of fixed carbon to N₂O reduction is superior to that of metal oxides. Char surface is relatively complex, but char active sites are mainly located at char edges. Kenshi Noda et al. [15] applied isotope gases to investigate the migration of nitrogen atom and concluded that carbon free sites can decompose N₂O into N₂ and residual oxygen adsorbed on char edge. The residual oxygen can react with char to generate CO. In detail, heterogeneous reduction of N₂O by char can be described as followings [15,16]:



Where C() is free active sites on char edge.

Furthermore, CO and temperature have a significant promotion effect on N₂O reduction by char. [11,12] Li et al. [11] studied the effect of temperature on N₂O reduction via changing the operating parameters and concluded that N₂O concentration can decrease from 90 mg/MJ to 40 mg/MJ when average temperature increases from 800 °C to 900 °C. Wang et al. [12] investigated the effect of CO on N₂O reduction applying synthetic coal and suggested that apparent activation energy of N₂O reduction decreases 21 kJ/mol with high concentration CO of 0.45%. Heterogeneous reduction of N₂O by char in the presence of CO can be expressed as followings [17]:



In both cases, according to the reaction process, heterogeneous reduction of N₂O by char can be divided into two stages: N₂O decomposition on char edge and residual oxygen desorption from char edge [16].

Although heterogeneous reduction reaction of N₂O by char can be described by R2 and R3 briefly, the detailed reaction process of heterogeneous reduction of N₂O by char in molecular level still remains obscure [17]. Understanding the micro-mechanism of N₂O reduction can serve to optimize N₂O reduction and lower N₂O emissions. However, few theoretical calculations have been conducted to investigate heterogeneous reduction of N₂O by char. Therefore, a contribution from quantum chemistry calculations is obviously essential to elucidate this unclear mechanism.

Quantum chemistry is one of the most reliable methods to investigate the microscopic mechanism of chemical reaction [18–21]. Kyotani et al. [18] studied the adsorption configuration of N₂O on carbonaceous surfaces using an ab initio molecular orbital theory. Arenillas et al. [19] clarified the micro reaction path of NO reduction by char in density functional theory (DFT) of quantum chemistry. Zhang et al. [21] evaluated thermodynamic and kinetic of the reduction reaction between NO and char nitrogen by DFT theoretical calculation and revealed the micro-mechanism between NO and char nitrogen. Therefore, theoretical calculation study on heterogeneous reduction of N₂O by char via quantum chemistry method is reasonable and imperative.

In this study, we focus on microscopic reaction pathways, energy barriers, thermodynamic and kinetic analysis by a combination of DFT and conventional transition state theory (TST). In addition, the microscopic mechanism of CO on N₂O heterogeneous

reduction by char is also investigated. The elementary reaction in this study can be expressed as followings:



where C(O) and Cd are surface oxygen species and defect in char edge, respectively. To the best of the author's knowledge, this is the first theoretical research on heterogeneous reduction of N₂O by char. The calculation results can not only clarify microscopic reaction process and provide necessary kinetic parameters for operation optimization of low N₂O emission, but also reveal the microscopic mechanism of CO on N₂O heterogeneous reduction by char.

2. Computational details

2.1. Choice of char edge model

Reasonably simplified char edge model is a critical factor for substantially accurate results [20]. According to the previous theoretical results, we can know that armchair and zigzag benzene rings are two typical research models of carbonaceous surfaces [22]. Chen and Yang [23,24] investigated the chemical properties of graphene models by quantum chemistry calculation and suggested that seven zigzag and six armchair benzene rings are suitable models for reaction mechanism research owing to parameters in excellent agreement with experimental data. In addition, many reaction mechanisms involving carbonaceous surfaces have been successfully investigated employing these two char edge models [25–27]. Therefore, it is reasonable to select six armchair and seven zigzag benzene rings as char edge models, as shown in Fig. 1.

2.2. Choice of calculation method

Calculation method and basis set are directly related to the accuracy of calculation results and the computational time, which are other important factors in quantum chemistry calculations. Geometry optimizations of reactants, intermediates (IM), transition states (TS) and products were performed at B3LYP/6-31G(d) level, and single point energy calculations for thermodynamic analysis were conducted at B2PLYP theory (double hybrid density functional) with Def2-tzvp level (all electron basis sets for the first four row elements) so as to obtain accuracy energy barrier value. Previous studies have shown that B3LYP/6-31G(d) not only can obtain a good calculation accuracy but also can reduce calculation time in chemical reaction calculation [28–31]. In terms of spin multiplicity effect, the lowest energy states determined from single point energy calculations at B3LYP/6-31G(d) level for several spin multiplicities [32]. In addition, frequency calculations were completed to check imaginary frequency and obtain zero point correction [26]. Furthermore, intrinsic reaction coordinate (IRC) calculations were conducted to confirm the right connection between each TS and corresponding IM. All quantum chemistry calculations were performed at Gaussian09 software package [33].

Kinetic analysis of each reaction step was performed from 800 K to 1400 K by conventional TST [34], the equation is as following:

$$k^{TST} = \Gamma \times \frac{k_B T}{h} \times \frac{Q_{TS}}{Q_A Q_B} \times \exp\left(\frac{-E_b}{RT}\right) \quad (1)$$

where E_b is energy barrier of each reaction step, kJ mol⁻¹; R is universal gas constant, J mol⁻¹ K⁻¹; T is reaction temperature, K; k_B is Boltzmann constant, J K⁻¹; h is Planck constant, J s; Q_{TS} , Q_A and Q_B are partial function of transition state TS , reactant A and reactant B ,

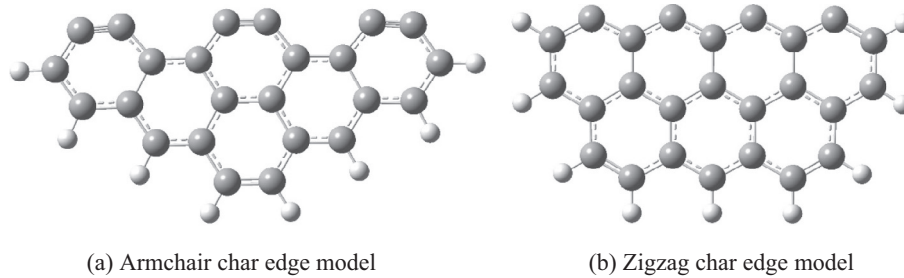


Fig. 1. char edge models.

respectively; Γ is quantum tunneling correction factor, which can be calculated by following equation:

$$\Gamma = 1 + \left(\frac{1}{24}\right) \times \left(\frac{h\nu_m c}{k_B T}\right)^2 \quad (2)$$

where ν_m is the imaginary frequency of transition states, cm^{-1} ; c is light speed, m s^{-1} .

Equilibrium constant can be acquired through the following equation [35]:

$$\Delta G = G_B - G_A = -RT \ln K \quad (3)$$

where G_A and G_B are Gibbs free energy of reactants and products, kJ K^{-1} ; K is equilibrium constant.

3. Results and discussion

In this section, heterogeneous reductions of N_2O based on armchair and zigzag char edge models are calculated and discussed respectively. The first step of heterogeneous reduction is the adsorption process of gases on char edge, gas concentration has an important effect on the competitive adsorption process of gas at char edges. However, understanding the reaction mechanism between gases adsorbed on char edge and char edge is the main goal of this study. Therefore, the gas concentration effect on heterogeneous reductions of N_2O is not considered in this work. In each char edge model, different adsorption configurations of N_2O on carbonaceous surfaces are considered and the most stable adsorption configuration is chosen to study heterogeneous reductions of N_2O . Furthermore, heterogeneous reduction of N_2O is divided into two stages to analyze, the stage of N_2O decomposition and the stage of residual oxygen desorption. In detail, the stage of residual oxygen desorption has two different situations depending on whether there is CO.

3.1. N_2O reduction on armchair char edge model

Optimized structures of reactants, products, IM, and TS in heterogeneous reduction of N_2O by char are shown in Fig. 2, and corresponding reaction potential energy surfaces are schematic in Fig. 3. In addition, imaginary frequency value, vibration direction, Mulliken atomic charge and bond length are given in Fig. 2.

3.1.1. N_2O decomposition on armchair char edge

As shown in Fig. 3, the stage of N_2O decomposition on char edge undergoes three transition states, and N_2 is separated from char edge with residual oxygen on char edge. Molecular structures in the reaction process can be obtained in Fig. 2. Firstly, N_2O molecular attack carbon free sites on the char edge, and N_2O adsorbs on char edge with the decrease of distance between N_2O and char edge. N_2O adsorption on char edge is a lower energy barrier (38.42 kJ/mol) and high exothermic (314.23 kJ/mol) step. Secondly, with $\text{N}-\text{O}$ bond length increasing, N_2O decomposes into N_2 and

oxygen atom adsorbed on char edge (1.497 \AA (IM1) \rightarrow 2.063 \AA (TS2) \rightarrow 3.201 \AA (IM2)), which is almost barrier less (9.20 kJ/mol). Finally, N_2 desorption from char edge occurs is a higher-barrier(151.90 kJ/mol) step, with $\text{N}-\text{C}(2)$ bond length increasing (1.324 \AA (IM2) \rightarrow 2.407 \AA (TS3) \rightarrow 3.658 \AA (IM3)).

3.1.2. Oxygen desorption from armchair char edge

As described in Fig. 3, residual oxygen combines with CO in fuel gas into CO_2 is presented as red lines, and residual oxygen reacts with char edge into CO is expressed as blue lines. In the presence of CO, CO molecule adsorbs on char(O) surface with a large exothermic (164.84 kJ/mol) firstly, and adsorption configuration is similar to the structure of CO_2 adsorption on char edge [36]. Subsequently, residual oxygen combined with CO desorbs from char edge with a medium energy barrier (147.96 kJ/mol), and $\text{C}-\text{O}$ bond length gradually extends in the desorption process can be seen in Fig. 2.

In the absence of CO, a novel reaction route for residual oxygen desorption from char edge is proposed in armchair char edge, as illustrated in Fig. 2. Firstly, residual oxygen reacts with carbon free sites in char edge into CO molecule through a small energy barrier (30.99 kJ/mol), and char edge deforms from hexagonal into pentagon in this process. Secondly, CO desorption from char edge occurs with a very high energy barrier (306.00 kJ/mol), forming a deformed char edge model (named as Cd1). This CO desorption process is available to accomplish under high temperature environment such as circulating fluidized bed. It is remarkable that ground state of armchair char edge model is singlet while that of Cd1 is triplet. In addition, Mulliken atomic charge of Cd1 is presented in Fig. 2. From Mulliken atomic charge of Cd1, C(2) in the middle of Cd1 contains bigger charge value compared with other carbon atoms in both sides, which may indicate that C(2) has higher reaction activity.

Comparing energy barrier value of two different oxygen desorption routes, residual oxygen desorption with CO is more likely to occur, which reveals that CO in flue gas favors residual oxygen desorption. According to energy barrier value of reaction steps, reaction rate-determining step can be identified. Rate-determining step of N_2O decomposition, which is N_2 desorption from char edge, is from IM2 to IM3. For residual oxygen desorption from char edge, rate-determining steps are from IM7 to IM8 (with CO) and from IM10 to IM11 (without CO), respectively.

3.2. N_2O reduction on zigzag char edge model

Optimized structures of N_2O heterogeneous reduction on zigzag char edge model are shown in Fig. 4, and corresponding reaction potential energy surfaces are schematic in Fig. 5. In addition, imaginary frequency value, vibration direction, Mulliken atomic charge and bond length are given in Fig. 4. Similar to N_2O reduction on armchair char model, heterogeneous reduction includes two stages, N_2O reduction on char edge and oxygen desorption from char edge, which are discussed particularly in this section.

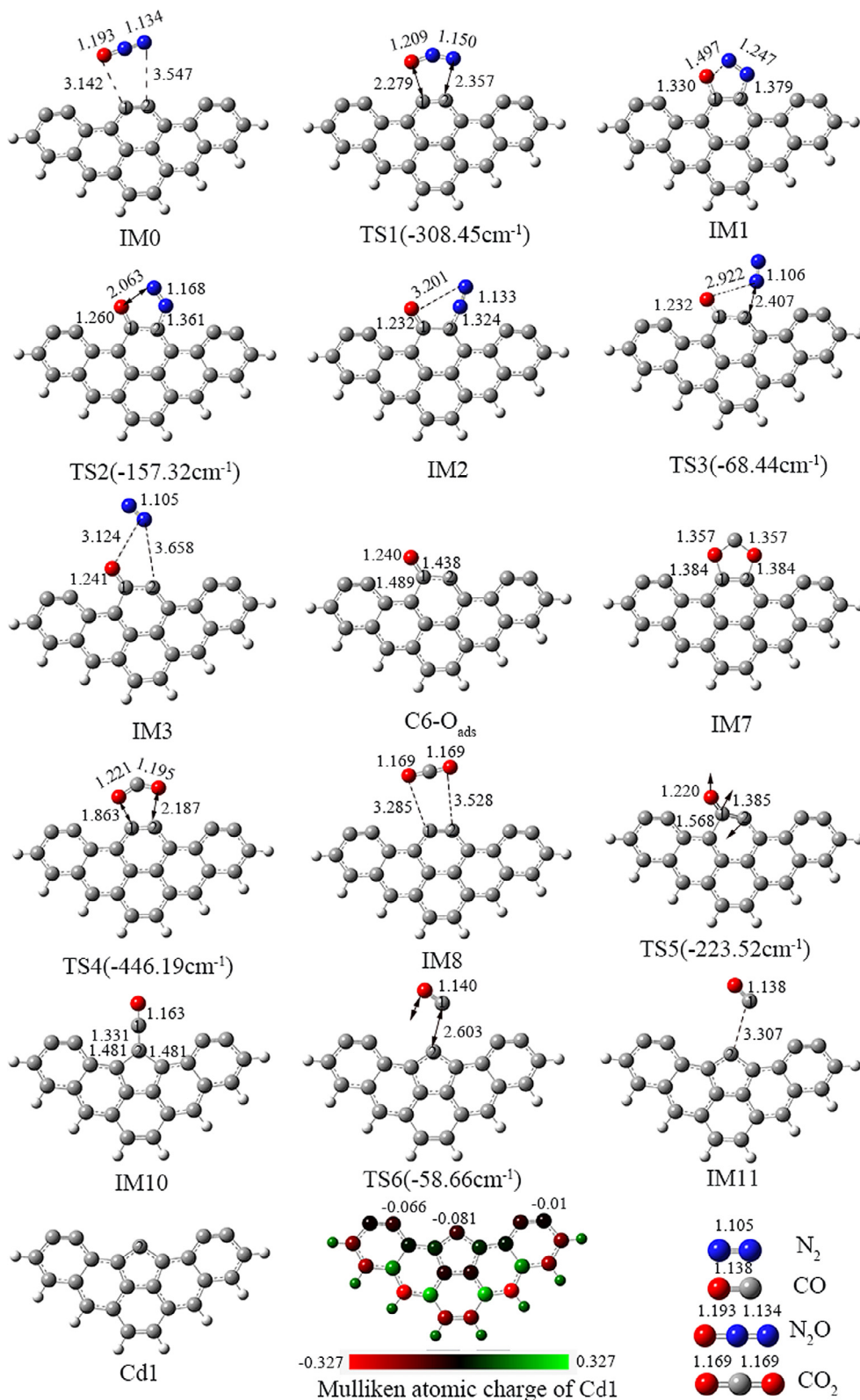


Fig. 2. Optimized structures of stable stationary points for N_2O reduction on armchair model. Bond lengths in Angstroms. ($1 \text{ \AA} = 10^{-10} \text{ m}$).

3.2.1. N_2O decomposition on zigzag char edge

From Fig. 5, the stage of N_2O decomposition on char edge occurs via three transition states. Firstly, N_2O molecule adsorbs on char edge with a large exothermic (-403.35 kJ/mol). Comparing N–O bond length of N_2O molecule and N_2O adsorbed on zigzag char edge (1.193 \AA vs 1.508 \AA), N_2O adsorption on zigzag char edge

belongs to dissociative adsorption, which is similar to CO_2 and $HgCl$ adsorption on zigzag char edge [37,38]. Secondly, with N–O bond length increasing, N_2O decomposes into N_2 and residual oxygen adsorbed on char edge (1.508 \AA (IM0) \rightarrow 1.830 \AA (TS1) \rightarrow 3.063 \AA (IM1)), which is a small energy barrier (27.53 kJ/mol). Thirdly, N_2 adsorbed on char edge undergoes a minor deformation

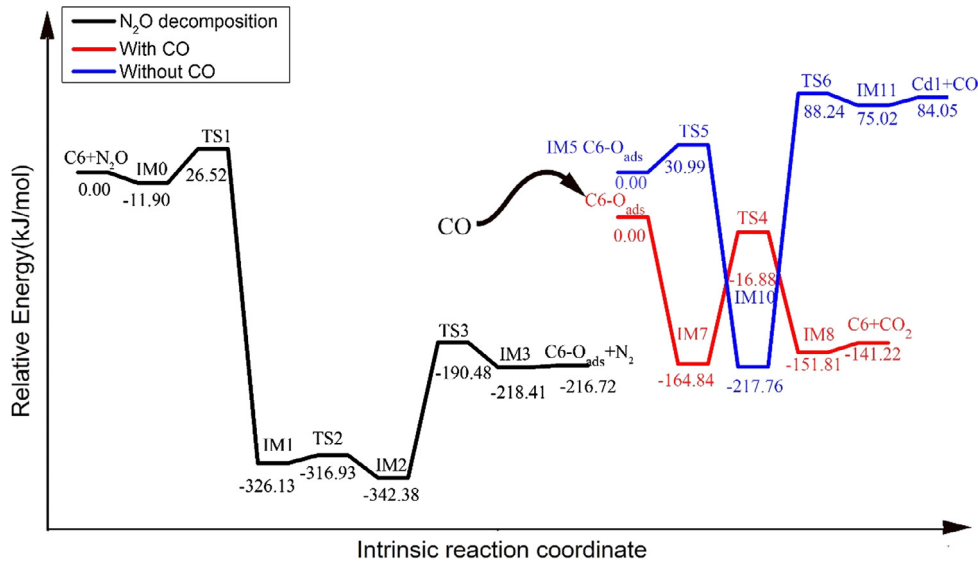


Fig. 3. Potential energy surfaces for N₂O reduction on armchair model.

via a small energy barrier (26.88 kJ/mol) while N–N bond and C–N bond are slightly stretched owing to activation of char edge (N–N: 1.146 Å(IM0) → 1.164 Å(TS1) → 1.181 Å(IM1), C–N: 1.340 Å(IM0) → 1.385 Å(TS1) → 1.440 Å(IM1)). Finally, N₂ desorption from char edge occurs with N–C bond length stretching (1.440 Å(IM1) → 1.871 Å(TS2) → 3.614 Å(IM2)), which is a lower energy barrier (39.94 kJ/mol) step.

3.2.2. Oxygen desorption from zigzag char edge

Similar to armchair model, oxygen desorption from char edge is classified into two different situations depending on whether CO exists. Residual oxygen desorption with CO is presented in green lines, while this desorption process without CO is described as blue and red lines. It is noteworthy that spin multiplicity also has significant influence on residual oxygen desorption stage in the absence of CO.

In the presence of CO, CO molecule adsorbs on char(O) surface, and this adsorption configuration is the same to CO₂ adsorption on zigzag char edge.[37] Subsequently, with the dihedral angle of CO and char edge increasing (0°(IM11) → 44.43°(TS6) → 108.48°(IM12)), oxygen atom (O2) desorbs from char edge with a medium energy barrier (181.38 kJ/mol). Finally, desorption of CO₂ and char edge occurs via a 193.81 kJ/mol energy barrier, with O1–C3 bond length increasing (1.413 Å(IM12) → 1.839 Å(TS7) → 3.502 Å(IM13)).

In the absence of CO, two different spin multiplicity reactions experience only one transition state to complete residual oxygen desorption. Residual oxygen react with carbon atom in char edge surface into CO and defect char edge (Cd2) through a high energy barrier (245.32 kJ/mol) in two spin multiplicity reaction, while similar reaction undergoes a higher energy barrier (364.39 kJ/mol) to generate CO and another defect char edge (Cd3) in four spin multiplicity reaction. Comparing two different spin multiplicity reaction energy barrier values, two spin multiplicity reaction is more likely to occur. In addition, Mulliken atomic charge of two kinds defect char edges are presented in Fig. 4.

Analyzing heterogeneous reduction of N₂O by char, char plays a catalytic role and provides reaction sites for N₂O and CO in the presence of CO, while char react with residual oxygen into “defect char” and CO in the absence of CO. According to energy barrier value of reaction steps, reaction rate-determining step can be iden-

tified. Rate-determining step of N₂O decomposition is from IM2 to IM3, which is N₂ desorption from char edge. For oxygen desorption from char edge, rate-determining steps are from IM12 to IM13 (with CO), from IM5 to IM6 (without CO, spin = 2) and from IM5 to IM8 (without CO, spin = 4), respectively. Furthermore, comparing energy barrier magnitude of three different oxygen desorption routes, residual oxygen desorption with CO is more likely to occur which reveals that CO in flue gas favors residual oxygen desorption, revealing the microscopic mechanism of CO prompting the N₂O reduction in experiment [12].

Comparing N₂O decomposition on the two kinds of char edges, rate-determining steps are all N₂ desorption from char edge, indicating that N₂ desorption step is the key factor affecting reduction rate. Therefore, in order to acquire more thermodynamic information about this key stage, thermodynamic calculation of N₂O decomposition is performed in the Section 3.2. Additionally, kinetic analysis of each rate-determining steps is also conducted in the Section 3.3 so as to obtain kinetic parameters, such as pre-exponential factor and activation energy.

3.3. Thermodynamic of N₂O decomposition

Bed temperature is maintained between 950 and 1250 K with coal as fluidized bed material,[3] so thermodynamic parameters of N₂O decomposition are calculated at temperature range of 800–1400 K. Thermodynamic parameters such as enthalpy, entropy, Gibbs free energy and equilibrium constant are favor to understand reaction property, as shown in Table 1.

As illustrated in Table 1, enthalpy ΔH of N₂O decomposition on two char edge models at different temperatures are below zero, confirming that N₂O decomposition process is an exothermic reaction. In detail, N₂O decomposition on zigzag char edge model emits more thermal energy compared with armchair char edge model, and exothermic magnitude is about 470 kJ/mol. Gibbs free energy ΔG of N₂O decomposition on two char edge models at different temperatures are below zero, revealing that N₂O decomposition process can happen spontaneously at research temperatures. Moreover, equilibrium constants of N₂O decomposition on two char edge models at different temperatures are all higher than 10⁵, suggesting that N₂O decomposition process can be carried out completely and take place irreversibly.

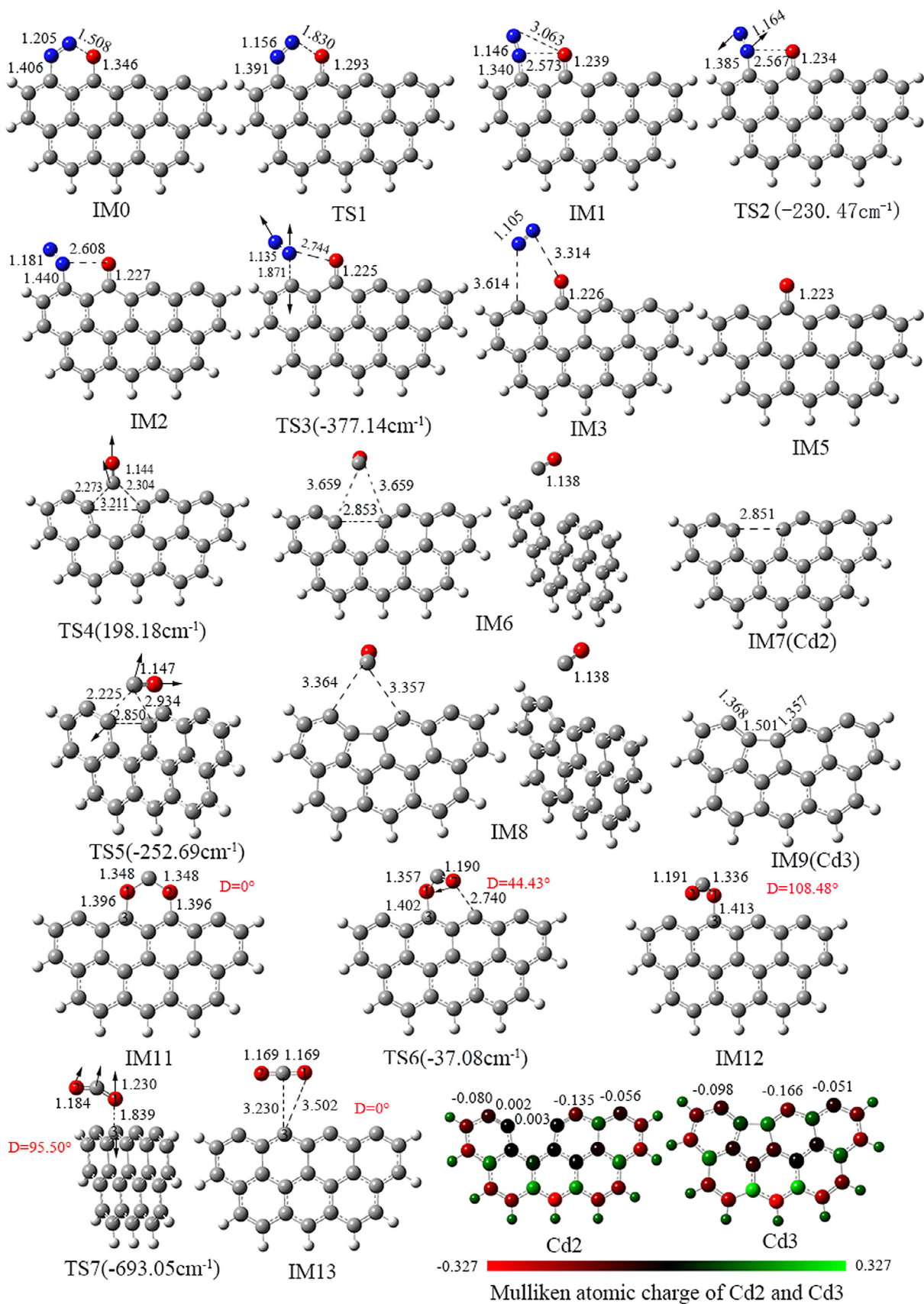


Fig. 4. Optimized structures of stable stationary points for N₂O reduction on zigzag model. Bond lengths in Angstroms.

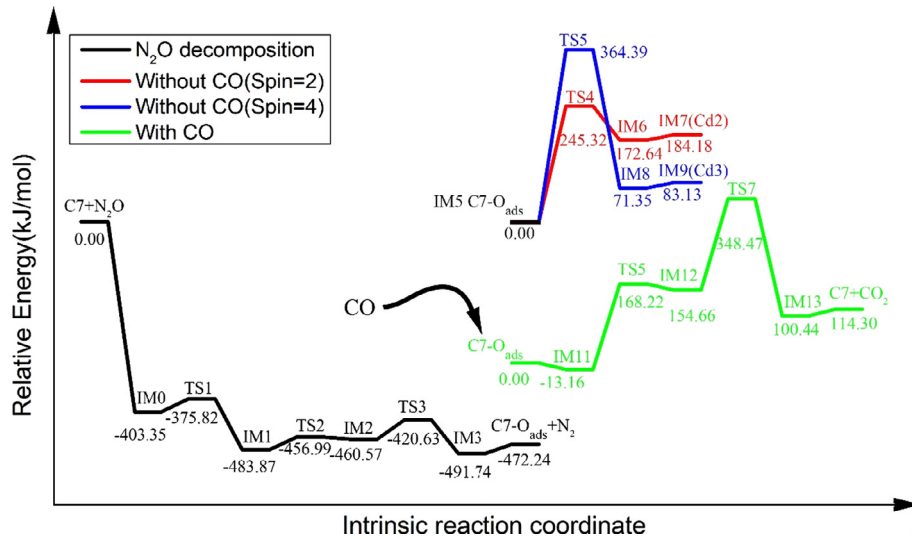


Fig. 5. Potential energy surfaces for N_2O reduction on zigzag model.

Table 1
Thermodynamic parameters at different temperatures.

Temperature (K)	C6-Armchair				C7-Zigzag			
	ΔH (kJ·mol ⁻¹)	ΔS (J·mol ⁻¹ ·K ⁻¹)	ΔG (kJ·mol ⁻¹)	K	ΔH (kJ·mol ⁻¹)	ΔS (J·mol ⁻¹ ·K ⁻¹)	ΔG (kJ·mol ⁻¹)	K
800	-205.84	-0.71	-205.18	2.50×10^{13}	-470.91	-6.68	-465.58	2.52×10^{30}
900	-205.66	-0.50	-205.12	8.03×10^{11}	-471.08	-6.88	-464.91	9.63×10^{26}
1000	-205.50	-0.33	-205.08	5.15×10^{10}	-471.25	-7.06	-464.21	1.77×10^{24}
1100	-205.35	-0.19	-205.05	5.46×10^{09}	-471.41	-7.21	-463.49	1.02×10^{22}
1200	-205.22	-0.08	-205.04	8.42×10^{08}	-471.56	-7.34	-462.77	1.40×10^{20}
1300	-205.10	0.02	-205.03	1.73×10^{08}	-471.69	-7.44	-462.03	3.67×10^{18}
1400	-204.99	0.10	-205.04	4.47×10^{07}	-471.81	-7.54	-461.28	1.63×10^{17}

3.4. Kinetics of the reaction between N_2O and char

Kinetics analysis can acquire reaction rate constant and lay the foundation for prediction model. According to Eqs. (1) and (2), the calculated reaction rate constants of rate-determining steps are plotted in Fig. 6, and rate constants based on armchair and zigzag char edge surface models are plotted with solid lines and dotted lines, respectively. Besides, corresponding Arrhenius parameters acquired from fitting the reaction rate constants are tabulated in Table 2.

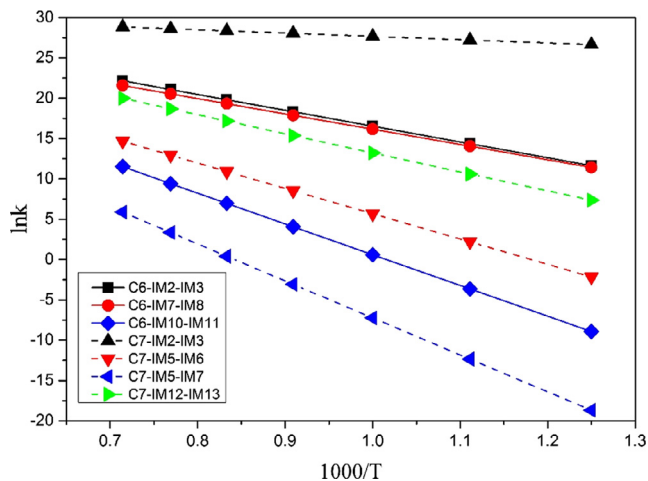


Fig. 6. Reaction rate constants for rate-determining steps.

From Fig. 6, reaction rate constants increase with the increase of temperature, revealing that heterogeneous reduction of N_2O by char is largely affected by the temperature which is consistent with experimental results that a higher combustion temperature contributes to lower N_2O emission [12,16]. Rate constants of oxygen desorption are lower than N_2 desorption, because activation energy of oxygen desorption is higher than N_2 desorption in general, as shown in Table 2. Rate constant of N_2 desorption from zigzag char edge is greatest, which is in agreement with the smallest activation energy (33.91 kJ/mol).

Comparing activation energy values of oxygen desorption with CO and without CO, activation energy of oxygen desorption with CO is much lower than that without CO, revealing that CO can reduce reaction energy barrier. From the microscopic reaction process and kinetics calculation results, Wang et al. [12] experimental phenomena can be well explained in molecular level and the heterogeneous reduction mechanism of N_2O by char is deepened in further. In addition, the promotion effect of CO on N_2O reduction is consistent with theoretical calculation results on other catalyzer [9].

Furthermore, for activation energy of homogeneous reaction between N_2O and CO, experimental and theoretical results are 184.10 and 277.82 kJ/mol respectively which are higher than N_2O decomposition on char edge [17,39], revealing that char edge can not only provide reaction location but also reduce the reaction energy barrier.

In Table 2, activation energy of N_2O decomposition on zigzag char edge is lower than armchair char edge (33.91 kJ/mol vs 163.58 kJ/mol), which is mainly due to the activity of free sites on char edge. Previous theoretical study indicated that zigzag char

Table 2
Kinetic parameters for rate-determining steps.

Char edge	Stages	Reaction steps	Pre-exponential factor A	Activation energy Ea (kJ·mol ⁻¹)	Arrhenius equations
Armchair	N ₂ O decomposition	IM2 → IM3	5.33 × 10 ¹⁵	163.58	5.33 × 10 ¹⁵ exp(-19675.25/T)
	Oxygen desorption (CO)	IM7 → IM8	1.79 × 10 ¹⁵	157.72	1.79 × 10 ¹⁵ exp(-18970.41/T)
	Oxygen desorption	IM10 → IM11	6.91 × 10 ¹⁶	317.41	6.91 × 10 ¹⁶ exp(-38177.77/T)
Zigzag	N ₂ O decomposition	IM2 → IM3	6.10 × 10 ¹³	33.91	6.10 × 10 ¹³ exp(-4078.66/T)
	Oxygen desorption (Spin = 2)	IM5 → IM6	1.30 × 10 ¹⁶	261.23	1.30 × 10 ¹⁶ exp(-31420.50/T)
	Oxygen desorption (Spin = 4)	IM5 → IM8	5.95 × 10 ¹⁶	381.29	5.95 × 10 ¹⁶ exp(-45861.20/T)
	Oxygen desorption (CO)	IM12 → IM13	1.02 × 10 ¹⁶	196.44	1.02 × 10 ¹⁶ exp(-23627.62/T)

edge has higher reaction activity compared with armchair [23,40], so similar reaction processes on the two kinds of char edges are significantly different in activation energy value. Furthermore, activation energy of N₂O decomposition on char edge is about at the range of 66–115 kJ/mol in precious experimental research [16], while the calculation results in the current study are 33.91 and 163.58 kJ/mol. In practical coal combustion environment, two kinds of char edge models exist at different proportion and their comprehensive apparent activation energy magnitude could be consistent with the experimental results. Therefore, in order to acquire accurate calculation results, different calculation models should be taken into account, especially in the investigation of N₂O heterogeneous reduction by char.

4. Conclusion

Reaction pathways, thermodynamic and kinetics calculation have been performed in the present work to investigate the heterogeneous reduction of N₂O by char via density functional theory. Stemming from the above calculated results and discussion, five conclusions can be conclude by the following:

- (1) Heterogeneous reduction of N₂O by char undergoes two stages, N₂O decomposition on char edge and residual oxygen desorption from char edge. N₂O decomposition on the two kinds of char edges experiences similar reaction process, while oxygen desorption from the two kinds of char edges accomplishes via obviously different paths.
- (2) N₂O decomposition process is an exothermic reaction and takes place spontaneously and irreversibly at the operating temperature of circulating fluidized bed.
- (3) In the presence of CO, char acts as an important catalyst which not only provides free sites as reaction location but also reduce the reaction energy barrier. In the absence of CO, char reacts with residual oxygen absorbed on char edge into CO molecule via a higher energy barrier.
- (4) The participation of CO can significantly reduce reaction activation energy of residual oxygen desorption and promote reaction rate of heterogeneous reduction of N₂O by char.
- (5) Char edge structure has notable influence on activation energy of N₂O decomposition on char edge. Activation energy values of N₂O decomposition on zigzag and armchair char edge are 33.91 kJ/mol and 163.58 kJ/mol, respectively.

For further studies, it may be of interest to investigate the effect of CO and residual oxygen on N₂O decomposition stage. Gas concentration effect on competitive adsorption process should be investigated in order to improve this heterogeneous reduction mechanism. In addition, in light of diversity and complexity of char edge in real combustion process, similar theoretical calculations of the current study on defect char and char nitrogen should be performed to provide further insight into the detail mechanism of N₂O heterogeneous reduction by char.

Acknowledgement

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